

**IN THE SPECIFICATION:**

Kindly amend WO2004/113590 at page 6, lines 5 – 25:

The electrolyte flows in the prior art EC or FC at constant flow rate. According to the present invention in an ETC the flow rate is varied by modulating the pressure of the electrolyte. The electrodes of an ETC are those known in the art. They are porous and formed in sandwich multilayer assembly, by juxtaposition and heat sinterised under pressure, on a metallic mesh which will later constitute the electric conductor. The mesh is to be found on the gas side. The different layers present hydrophobic layers with macroporous and micro-porous matrix containing hydrophilic metal-catalytic clusters. The electrodes constituents can be for instance mixtures of carbon powders and PTFE (politetrafluorineethylene) or similar binders. The ratio binders/carbon powders is higher in the layers close to gas side and the metallic mesh connectors and lower on the side of the alkaline electrolyte, where the layers are richer in carbon catalytically activated by metals and compounds known in the art. The electrodes, used for the AEG EC, further present for both cathode and anode on the electrolyte side a non-conductive and non-catalytic, preferably hydrophilic, layer. The porous electrodes are weeping at the gas side in the form of drops. The electrolyte drops are recycled into the electrolytic cell.

The pulsating flow of the electrolyte within the porous electrodes is produced by two opening/closing valves operating on the inlet and in the outlet of the electrolyte to/from a module or to/from the cells modules battery.

Considering P the pressure of the gases at the anode or cathode side, the valve at the electrolyte inlet side produces an overpressure  $p + dp$   $P + dP$  and alternatively the valve at the electrolyte outlet side an overpressure  $p - dp$   $P - dP$ , where  $dP > dp$ .